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9th, 10th, NEET, JEE(Main/Advanced)

अभ्यास ही सबसे बड़ा गुरु है।

CLASS : XI (PHYSICAL CHEMISTRY)

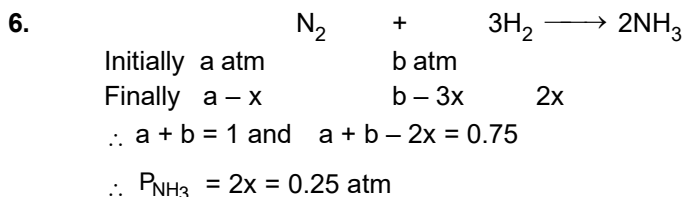
D P P

DAILY PRACTICE PROBLEM

Solutions (PART-II)

DPP-32 to 59

DPP No. # 32

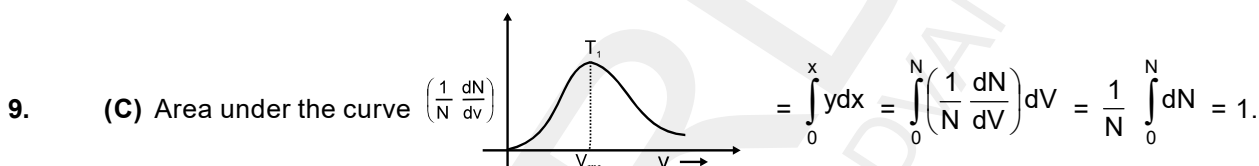


7.
$$V_{\text{RMS}} = \sqrt{\frac{3RT}{M}} = \sqrt{\frac{3P}{\rho}} = \sqrt{\frac{3 \times 1.2 \times 10^5}{4}} = 300 \text{ m/s}$$

8.
$$[(v_{\text{rms}})_x]_{546^\circ\text{C}} = [(v_{\text{mp}})_y]_{273^\circ\text{C}}$$

$$\sqrt{\frac{3RT_x}{M_x}} = \sqrt{\frac{2RT_y}{M_y}} \quad \frac{3 \times 819}{9} = \frac{2 \times 546}{M_y}$$

$\therefore M_y = 4 \text{ amu.}$



11. (C,D) If two gases have identical Maxwellian plot then their all the speeds will also be identical.

Hence $\frac{T_A}{M_A} = \frac{T_B}{M_B}$. Since all the speeds are proportional to $\sqrt{\frac{T}{M}}$

for $\text{SO}_2 - M_1 = 64, T_1 = 600 \text{ K}; \text{O}_2 - M_2 = 32, T_2 = 300 \text{ K} \Rightarrow \frac{T_1}{M_1} = \frac{T_2}{M_2}$.

DPP No. # 33

1. (a) V.P. depends on temperature.
 3. Pressure of air = 750 - 100 = 650 mm of Hg
 on compressing $P_f = \text{Hg } 650 \times 3 \text{ mm of Hg}$
 $= 1950 \text{ mm of Hg}$
 so $P_T = (1950 + 100) = 2050 \text{ mm of Hg}$
 4. $P_{\text{N}_2} + P_{\text{H}_2\text{O}(v)} = 1 \text{ atm}, \therefore P_{\text{H}_2\text{O}} = 0.3 \text{ atm}$
 $\therefore P_{\text{N}_2} = 0.7 \text{ atm}$

Now new pressure of N_2 in another vessel of volume $V/3$ at same T is given by :

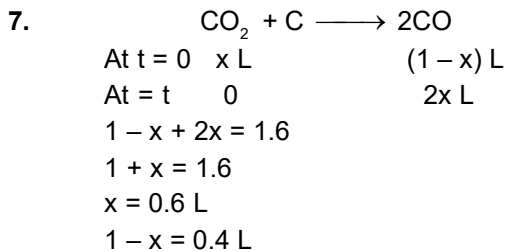
$$P_{\text{N}_2} \times \frac{V_1}{3} = 0.70 \times V_1$$

$\therefore P_{\text{N}_2} = 2.1 \text{ atm}$

Since aqueous tension remains constant, and thus total pressure in new vessel.

$$= P_{\text{N}_2} + P_{\text{H}_2\text{O}} = 2.1 + 0.3 = 2.4 \text{ atm.}$$

5.
$$3\text{O}_2 \rightleftharpoons 2\text{O}_3$$
- t = 0 60
 t = t_1 48 8
 so $V_1 = 48 + 8 = 56$ and $V_2 = 48$ (on passing through turpentine oil, O_3 will be absorbed.)



8. 896 mL.

DPP No. # 34

1. $T_4 < T_3 < T_2 < T_1$

2. A real gas behaves ideally under conditions of low pressure and high temperature.

3. Order of Vander waals constant $\text{CO}_2 > \text{CH}_4 > \text{N}_2 > \text{H}_2$
 \therefore ease of liquification $\text{CO}_2 > \text{CH}_4 > \text{N}_2 > \text{H}_2$

5.* Z for an ideal gas is equal one.

6. Clearly, from the graph at 80 K $= \frac{PV}{RT} = 1$ and at 60K, $Z < 1$

7. $Z = \frac{PV}{nRT} \Rightarrow n = \frac{PV}{ZRT}$

8. Translational energy $= (3/2) kT$
 $= (3/2) kT = hcR_H ((1/1) - (1/4))$

$$= (3/2) T = 6.626 \times 10^{-34} \times 2.996 \times 10^{10} \times 109679 \times (3/4) \frac{6.02 \times 10^{23}}{8.315}$$

$$= 118331.1 \text{ K}$$

$$T = 118331.1 \times 2/3 = 80000 \text{ K.}$$

DPP No. # 35

4. For very large value of molar volume (V_m)

$\frac{a}{V_m}$ and b can be neglected, so gas behaves as Ideal

$$\therefore PV_m = RT$$

5. At low pressure vander waal's equivalent for a real gas is given as

$$Z = 1 - \frac{a}{RTV}$$

intercept = 1

slop = -ve

7. (i) $Z = \frac{PM}{dRT} = \frac{2 \times 16}{0.8 \times \frac{1}{12} \times 400} = 1.2$

(ii) As $Z > 1$, so repulsive forces are dominating among gas molecules.

8. At Boyle's temperature, for low pressure regions, $Z = 1$. However, for high pressure regions, $Z > 1$.

DPP No. # 36

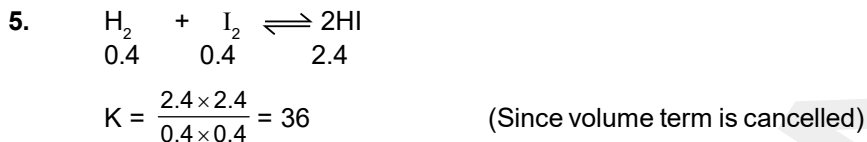
4. Under low pressure region and below the boyle temperature, $Z < 1$.

5. Refer class notes.

- 7.* at very high Pressure $Z = 1 + \frac{Pb}{RT}$
 $Z > 1$
 for particular real gas above boyle temp $Z > 1$.

8. $[A - r] ; [B - r, s] ; [C - q] ; [D - r]$.

DPP No. # 37



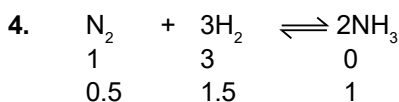
7. Mol. mass of HI = 1 + 127 = 128
 64 g HI = 64 / 128 = 0.5 mole

$$[\text{HI}] = \frac{0.5}{2} \quad M = 0.25 \text{ M}$$

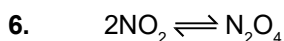
DPP No. # 38

1. $K_p = K_c (RT)^{\Delta n}$
 $2K_c = K_c (RT)^{\Delta n}$
 $2 = (RT)^1$

$$T = \frac{2}{0.0821} = 24.36 \text{ K}$$



$$P_{\text{H}_2} = \frac{1.5}{3} P = P/2$$



$$K_c = \frac{[\text{N}_2\text{O}_4]}{[\text{NO}_2]^2} = \left(= \frac{\text{mol L}^{-1}}{(\text{mol L}^{-1})^2}, K_c \text{ has unit of } \text{L mol}^{-1} \right)$$

$$K_p = \frac{P_{\text{N}_2\text{O}_4}}{P_{\text{NO}_2}^2} \left(= \frac{\text{atm}}{\text{atm}^2}, K_p \text{ has unit of } \text{atm}^{-1} \right)$$

(Since mole fraction is itself unitless hence, K_x is also unitless)

7. (i) Molar concentrations :

$$[\text{PCl}_5] = \frac{\text{mol}}{\text{L}} = \frac{1}{2} = 0.5 \text{ mol L}^{-1}$$

$$[\text{PCl}_3] = \frac{2}{2} = 1.0 \text{ mol L}^{-1}$$

$$[\text{Cl}_2] = \frac{2}{2} = 1.0 \text{ mol L}^{-1}$$

(ii) Mole fractions :

Total moles at equilibrium = 1 + 2 + 2 = 5

$$\therefore X_{\text{PCl}_5} = \frac{n_{\text{PCl}_5}}{n_{\text{total}}} = \frac{1}{5} = 0.2$$

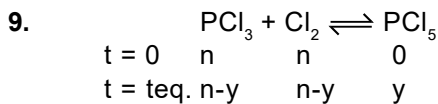
$$X_{\text{PCl}_3} = \frac{n_{\text{PCl}_3}}{n_{\text{total}}} = \frac{2}{5} = 0.4$$

$$X_{Cl_2} = \frac{n_{Cl_2}}{n_{total}} = \frac{2}{5} = 0.4$$

(iii) Equilibrium constants :

$$K_c = \frac{[PCl_3][Cl_2]}{[PCl_5]} = \frac{1 \times 1}{0.5} = 2 \text{ (mol L}^{-1}\text{)}^{-1} = 2 \text{ L mol}^{-1}$$

8. $K_c = 4.0.$

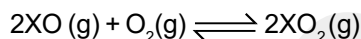


$$K_p = \frac{y}{(n-y)(n-y)} \left[\frac{P}{2n-y} \right]^{-1}$$

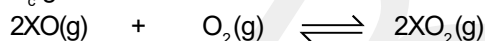
$$K_p = \frac{(2n-y)y}{(n-y)^2 P}$$

DPP No. # 39

8. The equilibrium reaction is



since the unit of K_c given is lit/mole.



Initial conc.	1	2	0
Conc. at equilib.	$1-2x$	$2-x$	$2x$

$$\therefore K_c = \frac{[XO_2]^2}{[XO]^2 [O_2]} = \frac{(2x)^2}{(1-2x)^2 (2-x)} = \frac{4x^2}{(1-2x)^2 (2-x)} = \frac{4x^2}{2}$$

Since, the value of equilibrium constant is very small (1×10^{-4}), so $2x$ can be ignored with respect to 1 and x can be ignored with respect to 2.

$$\therefore 1 \times 10^{-4} = \frac{4x^2}{2}$$

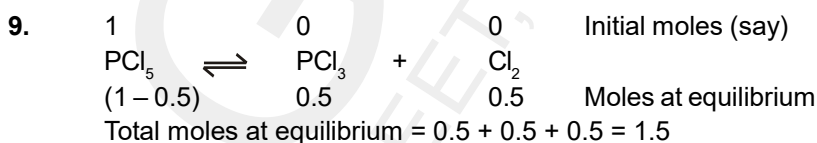
$$x = 7.07 \times 10^{-3}$$

we can see that the value of x is very small, so the assumption made was correct as it is within 1.4% of the actual value. Thus, the assumption made is correct and acceptable.

$$\therefore [XO] = 1 - 0.01414 = 0.985 \text{ M}$$

$$[O_2] = 2 - 0.00707 = 1.992 \text{ M}$$

$$[XO_2] = 0.0141 \text{ M}$$



$$K_p = \frac{p_{PCl_3} \cdot p_{Cl_2}}{p_{PCl_5}} = \frac{\left(\frac{0.5}{1.5}p\right) \left(\frac{0.5}{1.5}p\right)}{\left(\frac{0.5}{1.5}p\right)} \quad (p = \text{total pressure})$$

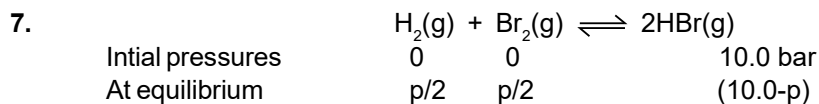
or $K_p = \frac{1}{3} \cdot p$ or $p = 3K_p.$

DPP No. # 40



At eqm. $2 - \frac{20}{100} \times 2$ 0.2 0.2
 $= 2 - 0.4 = 1.6$

$$K = \frac{[H_2][I_2]}{[HI]} = \frac{0.2 \times 0.2}{(1.6)^2} = \frac{1}{64}$$



$$K_p = \frac{p_{HBr}^2}{p_{H_2} \times p_{Br_2}}$$

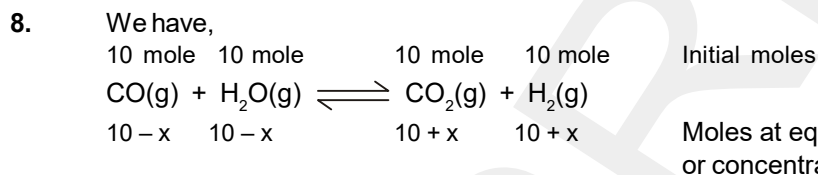
$$1.6 \times 10^5 = \frac{(10-p)^2}{(p/2)(p/2)}$$

Taking square root of both sides

$$4 \times 10^2 = \frac{10-p}{p/2}$$

$$200p = 10 - p; \quad p = \frac{10}{201} \text{ bar}$$

$$p_{H_2} = p/2 = \frac{1}{2} \left(\frac{10}{201} \right) \text{ bar} = 2.5 \times 10^{-2} \text{ bar}; \quad p_{Br_2} = p/2 = 2.5 \times 10^{-2} \text{ bar}; \quad p_{HBr} = 10 - p \approx 10 \text{ bar}$$



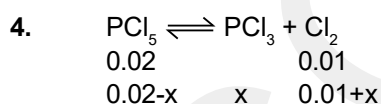
where x is the number of moles of each reactant changed to the products at equilibrium.

$$K = \frac{(10+x)^2}{(10-x)^2} = 9/4 \text{ (given)} \quad \text{or} \quad \frac{10+x}{10-x} = 3/2; \quad x = 2$$

$$\text{Mole percent of } H_2(g) \text{ at equilibrium} = \frac{10+x}{40} \times 100 = 30$$

DPP No. # 41

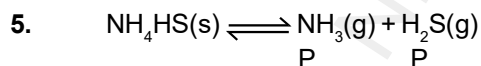
3. 0.2.



$$D = \frac{PM}{RT}$$

Calculate M_{avg} .

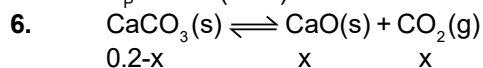
$$\frac{(0.02-x)208.5 + 137.5x + (0.01+x)71}{0.03+x} = M_{avg}$$



$$2P = 1.12$$

$$P = 0.56$$

$$K_p = P^2 = (0.56)^2 = 0.3136 \text{ atm}^2$$



$$K_p = P_{CO_2} = 1$$

$$x = \text{mole of } CO_2 = \frac{PV}{RT}$$

$$\text{Remaining mass of } CaCO_3 = (0.2 - x) 100 \text{ g.}$$

$$7. \quad [\text{CaO}] = \frac{P_{\text{CaO(s)}}}{M_{\text{CaO(s)}}} = \frac{1.12}{56} \times 1000$$

- 9.* Addition of solids have no effect on equilibrium and temperature favours endothermic direction while increasing pressure will shift equilibrium in backward direction as Δn_g is +ve.

DPP No. # 42

$$2. \quad K_p = (p_{\text{H}_2\text{O}})^4 = 2.56 \times 10^{-10} \text{ atm}^4$$

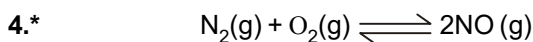
$$\therefore p_{\text{H}_2\text{O}} = 4 \times 10^{-3} \text{ atm} = 4 \times 10^{-3} \times 760 = 3.04 \text{ torr.}$$

$$\text{Partial pressure of water vapour in air} = \frac{40}{100} \times 12.5 = 5$$

So, the amount of water vapour in air should decrease to decrease value of partial pressure of water vapour from 5 torr to the equilibrium value (3.04 torr).

so, mass of $\text{CuSO}_4 \cdot 5\text{H}_2\text{O}$ will increase and mass of $\text{CuSO}_4 \cdot \text{H}_2\text{O}$ will decrease.

3. (A) As reaction is endothermic therefore it will go in the forward direction hence moles of PbO will increase.
(B) With the increase or decrease of volume partial pressure of the gases will remain same.
(C) Due to the addition of inert gas at constant pressure reaction will proceed in the direction in which more number of gaseous moles are formed.



(A) For changing pressure volume has to be changed, though number of moles of NO(g) do not get changed but its concentration will get changed.

(B) Temperature change will change K_p and hence concentration.

(C) Volume change will change concentration, not the number of moles.

(D) Catalyst does not change equilibrium concentrations.

- 5.* Number of moles will remain unchanged but due to decreased volume pressure will get increased and also the concentrations.

$$6. \quad \text{Slope} = -\tan 30^\circ = \frac{-1}{\sqrt{3}} = \frac{-\Delta H^\circ}{R}$$

$$\therefore \Delta H^\circ = \frac{R}{\sqrt{3}}$$

7. As $T \rightarrow \infty$, $K = A$

$$\therefore \ln A = \ln K = 46.06$$

$$\therefore 2.303 \log_{10} A = 46.06$$

$$\therefore A = 10^{20}$$

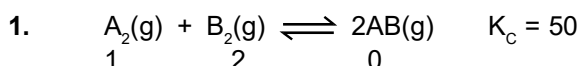
8. $\Delta H^\circ > 0$ \therefore Endothermic reaction

Y – intercept = +ve $\therefore \Delta S^\circ > 0$

for endothermic reaction, as $T \uparrow$, $K \uparrow$.

The value of equilibrium constant K is unaffected by pressure changes.

DPP No. # 43



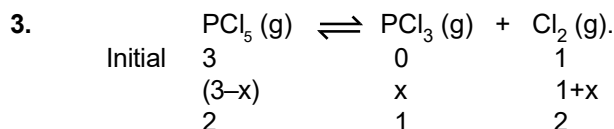
$$\begin{array}{ccc} 1-x & 2-x & 2x \\ 3 & 3 & 3 \end{array}$$

$$50 = \frac{\frac{2x}{3} \cdot \frac{2x}{3}}{\frac{1-x}{3} \cdot \frac{2-x}{3}} = \frac{4x^2}{(1-x)(2-x)} = \frac{4x^2}{2-3x+x^2} \Rightarrow 100 - 150x + 50x^2 = 4x^2$$

$$\therefore \text{no. of mol of AB} = \frac{2x}{3} = 1.868.$$

$$\therefore AB \text{ dh eksy la } ; k = \frac{2x}{3} = 1.868$$

2. (i) From the graph $0.3 \times n = 0.6$
 $n = 2$
 (ii) $K = (0.6)^2 / 0.3 = 1.2 \text{ mol / L}$



Initial total moles = (3+1) = 4.

Now from Ideal gas equation

$$PV = nRT = P \times 100 = 4 \times 0.082 \times 500$$

$$P = 0.082 \times 20 = 1.64 \text{ atm.}$$

At equilibrium Total mole = $3 - x + x + 1 + x = (4 + x)$

$$PV = nRT.$$

$$2.05 \times 100 = (4+x) \times 0.082 \times 500.$$

$$2.05 = (4+x) \times 0.41.$$

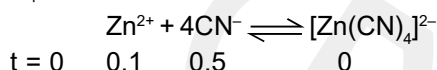
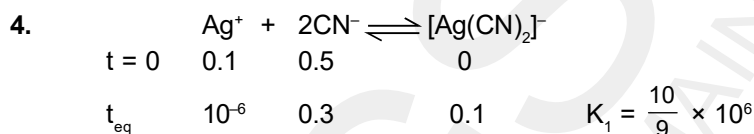
$$5 = 4 + x.$$

$$x = 1.$$

$$\alpha = \frac{\text{No. of mole dissociated}}{\text{Initially total mole taken}} = \frac{1}{3} = 0.33.$$

$$P_{PCl_5} = \frac{2}{5} \times 2.05 \quad ; \quad P_{PCl_3} = \frac{1}{5} \times 2.05 \quad P_{Cl_2} = \frac{2}{5} \times 2.05$$

$$K_p = \frac{\left(\frac{1}{5} \times 2.05\right) \left(\frac{2}{5} \times 2.05\right)}{\left(\frac{2}{5} \times 2.05\right)} = [0.41]$$



eq.	10^{-12}	0.1	0.1	$K_2 = \frac{0.1}{(0.1)^4 \times 10^{-12}} = 10^{15}$
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Subtracting two times Ist reaction from IInd reaction, we will get the required reaction, so

$$K_{eq} = \frac{10^{15}}{\left(\frac{10}{9}\right)^2 \times 10^{12}} = \frac{10^3 \times 81}{100} = 810 \quad \text{Ans. 810}$$

- 5.* When some amount of HCl is added to equilibrium, the first eq will shift in backward direction leading to decrease in amount of O₂. Then, the second eq. will shift in backward direction to increase the amount of O₂. Thus, amount of N₂ gas will increase.

DPP No. # 44

4. (i) Molecules move faster for which $\frac{T}{M}$ greater obviously H₂ molecule move faster.
5. State function : a, b, c, d, g, h, j ; Path function : e, f, i, k
6. Intensive : a, c, d, f, g, h, i, k ; Extensive : b, e, j, l
7. Open system : b, f, g, i, j ; Closed system : a, c, h ; Isolated system : d, e
8. Q = 7.5 KJ
 $\Delta U = -12 \text{ KJ}$
 $\Delta U = Q + W$
 $W = -12 - 7.5 = -19.5 \text{ KJ. Ans.}$
 Now W = 0,
 $\therefore \Delta U = Q \quad \therefore Q = \Delta U = -12 \text{ KJ Ans.}$

DPP No. # 45

5. $\Delta U_{ab} = Q_{abc} + W_{abc}$
 or $\Delta U_{ab} = 100 - 40 = 60 \text{ J}$
 $\Delta U_{ab} = Q_{aeb} + W_{aeb}$
 or $60 = Q_{aeb} - 20$
 or $Q_{aeb} = 80 \text{ J}$ **Ans.**

$\Delta U_{ba} = -60 \text{ J}$
 $W_{bda} = 30 \text{ J}$
 $\Delta U_{ba} = Q_{bda} + W_{bda}$
 or $Q_{bda} = \Delta U_{ba} - W_{bda}$
 or $Q_{bda} = -60 - 30 = -90 \text{ J}$ **Ans.**

Since Q_{bda} is (-)ve \therefore Heat is liberated from the system.

6. 4275 J.

7. 6.66 min. (400 sec)

8. Since $\Delta E = q + w$
 $= 80 - 30 = 50$

So for ADB

$\Delta E = q + w$
 $50 = q - 10$
 $q = 60 \text{ J}$

9. For B to A,
 $\Delta E = -50 \text{ J}$
 $w = +20 \text{ J}$
 $q = -50 - 20 = -70$

heat is liberate.

10. In ADB process, DB process is isochoric so $w_{DB} = 0$

So, $\Delta E_{AD} = q_{AD} + w_{AD}$
 $-40 = q_{AD} + (-10)$
 $q_{AD} = -30 \text{ J}$

Now, $q_{AB} = q_{AD} + q_{DB}$
 $60 = -30 + q_{DB}$
 $q_{DB} = 90 \text{ J}$

DPP No. # 46

1. $w = P_{\text{ext}} \Delta V$
 $w = -1.2 \times 32 = -38.4 \text{ lt atm.}$
 $= -38.4 \times 100 \text{ J} = -3840 \text{ J} = -3.84 \text{ kJ}$
 $\Delta E = q + w$
 so, $q = \Delta E - w = -51 + 3.84 = -47.16.$

6. $W = 240 \text{ L atm.}$

7. $\Delta U = \Delta H = 0$ $Q = -W$

$W = -2.303 nRT \log \frac{V_2}{V_1} \Rightarrow W = -2.3 \times \frac{20}{40} \times 8.3 \times 300 \log \frac{10}{5} = -859.05 \text{ J.}$

8. (a) $W = -nRT \ln \frac{V_2}{V_1}$
 $W = -P_1 V_1 \ln \frac{V_2}{V_1} = -14 \times 0.03 \ln \frac{0.06}{0.03} \text{ bar m}^3 = -14 \times 0.7 \times 0.03 = -0.294 \text{ bar m}^3 \text{ Ans.}$

(b) $P_1 V_1 = P_2 V_2$

$$\therefore P_2 = \frac{P_1 V_1}{V_2} = \frac{14 \times 0.03}{0.06} = 7 \text{ bar}$$

$$\therefore W = -P_{\text{ext}} (V_2 - V_1) = -7 (0.06 - 0.03) = -7 \times 0.03 = -0.21 \text{ bar m}^3.$$

$$\text{Efficiency} = \frac{0.21}{0.294} = 71.43\% \text{ Ans.}$$

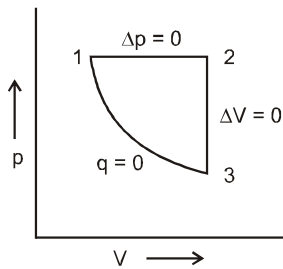
9. (a) F (b) T (c) F (d) T (e) T

DPP No. # 47

- The product PV is increasing so temperature will keep or increasing in the process, hence $\Delta H = \Delta E + \Delta(PV)$ will increase constantly.
- From graph we know that $V_B > V_A$, so expansion has taken place so w will be with -ve sign and ΔH will be +ve as both ΔE and $\Delta(PV)$ have increased.
- At A and D the temperatures of the gas will be equal, so $\Delta E = 0$, $\Delta H = 0$
Now $w = W_{AB} + W_{BC} + W_{CD} = -P_0 V_0 - 2P_0 V_0 \ln 2 + P_0 V_0 = -2P_0 V_0 \ln 2$
and $q = -W = 2P_0 V_0 \ln 2$
- Since liquid is expanding against external pressure P_0 hence work done
 $w = -P_0 (4V_0 - V_0) = -3P_0 V_0$
 $\Delta U = w = -3P_0 V_0$
 $\Rightarrow \Delta H = \Delta U + P_2 V_2 - P_1 V_1 = -3P_0 V_0 + 4P_0 V_0 - 2P_0 V_0$.
- γ for $O_2 = 1.44$ γ for He = 1.66.
- Since, ΔH is a state function, and the final state attained by the gas is same as its initial state, so value of $\Delta H = 0$.
- $q = q_{AB} + q_{BC} + q_{CD} + q_{DA}$
 $= -1R \times 300 \ln 2 + 1 \times \frac{5R}{2} \times (400 - 300) + 1R \times 400 \ln 2 + 1 \times \frac{5R}{2} \times (300 - 400)$
($\because q_{AB} = -W_{AB} = -1R \times 300 \ln 2$ since process is reversible isothermal for which $\Delta U = 0$).
($\because q_{BC} = \Delta H_{BC} = 1 \times \frac{5R}{2} \times (400 - 300)$ since process is reversible isobaric).
($\because q_{CD} = -W_{CD} = 1R \times 300 \ln 2$ since process is reversible isothermal for which $\Delta U = 0$).
($\because q_{DA} = \Delta H_{AB} = 1 \times \frac{5R}{2} \times (300 - 400)$ since process is reversible isobaric).
So, $q = 100 R \ln 2$.
- Since, for a cyclic process, $\Delta U = 0$.
So, $W = -q = -100 R \ln 2$.

DPP No. # 48

- $TV^{\gamma-1} = \text{constant}$
 $\gamma = \frac{5}{3} \quad \therefore \gamma - 1 = \frac{2}{3}$
 $\therefore 300 \times (8)^{2/3} = 250 \times (V_2)^{2/3} \Rightarrow (V_2)^{2/3} = 4.8$
 $\Rightarrow V_2 = (4.8)^{3/2} \cong 4.8 \times 2.2 = 10.5 \text{ L}$
- $\gamma_{\text{mix}} = \frac{n_A C_{PA} + n_B C_{PB}}{n_A C_{VA} + n_B C_{VB}} = \frac{2(4R) + 4(5R/2)}{2(3R) + 4(3R/2)} = \frac{18R}{12R} = \frac{3}{2}$
 $T_1 V_1^{\gamma-1} = T_2 V_2^{\gamma-1} \quad (\gamma = \gamma_{\text{mix}} = 1.5)$
 $\therefore T_2 = 320 \left(\frac{2}{8}\right)^{1.5-1} = 320 \times \frac{1}{2} = 160 \text{ K}$
 $\therefore W = \frac{nR}{\gamma-1} (T_2 - T_1) = \frac{6R}{1.5-1} (160 - 320) = -1920 R = 1920 \times 2 = -3840 \text{ calories.}$
- The process can be described on a p-V diagram as



At 1 : $p = 10 \text{ atm}$ $T = 400 \text{ K}$

At 2 : $p = 10 \text{ atm}$ $T = 800 \text{ K}$

At 3 : $p = ?$ $T = T_3$

$V = V_1$

$V = V_2 = 2V_1$

$V = V_3 = V_2 = 2V_1$

Therefore,

$W_{12} = -p\Delta V = -nRT = -400 R$

$W_{23} = 0$

[$\because \Delta V = 0$]

Between 3 and 1 ; $TV^{\gamma-1} = \text{constant}$

$T_3 (2V_1)^{\gamma-1} = 400(V_1)^{\gamma-1}$

$\Rightarrow T_3 = 400 \left(\frac{1}{2}\right)^{2/3} = 252 \text{ K}$

$\Rightarrow W_{31} = \Delta E_{31} = nC_V(T_1 - T_3) = \frac{3}{2} R(400 - 252) = 222 R$

$\Rightarrow W_{12-31} = W_{12} + W_{23} + W_{31} = -178 R$

10. $W = -\int PdV$

$= -\int \frac{K}{V^n} dV = -\frac{K}{1-n} [V^{-n+1}]_{V_1}^{V_2} = \frac{K}{n-1} [V_2^{1-n} - V_1^{1-n}]$

$= \frac{P_1 V_1^n}{n-1} [V_2^{1-n} - V_1^{1-n}] = \frac{P_1 V_1^{n+1-n}}{n-1} \left[\left(\frac{V_2}{V_1}\right)^{1-n} - 1 \right]$

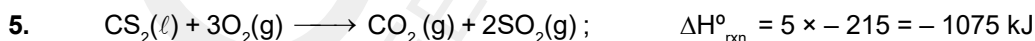
DPP No. # 49

1. Standard molar enthalpy of formation (ΔH_f°) of element in their stable state of aggregation is zero.

$\therefore \Delta H_f^\circ (\text{O}_2, \text{g}) = 0$

4. Some of the heat is used to vaporise the $\text{H}_2\text{O} (\ell)$

$\therefore x_1 > x_2$



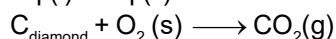
$\Delta H_{\text{rxn}}^\circ = \Delta H_f^\circ (\text{CO}_2) + 2 \times \Delta H_f^\circ (\text{SO}_2) - \Delta H_f^\circ (\text{CS}_2)$

$\Delta H_{\text{rxn}}^\circ = (-393.5 - 2 \times 296.8) - (-1075)$

$\Delta H_{\text{rxn}}^\circ = 87.9$

6. Refer Class notes.

8. Eq (i) + Eq (ii)



$\Delta H = \Delta H_1 + \Delta H_2$

DPP No. # 50

2. Since it is neutralisation of a weak acid with strong base.

3. enthalpy of dissociation = $(13.7 - 3) \text{ KCal} = 10.7 \text{ KCal}$

$$6. \quad n_{\text{CH}_4} = \frac{280}{22.4}$$

$$\therefore \Delta H_{\text{obtained}} = \frac{240 \times 280}{22.4} \text{ KCal}$$

$$\therefore m = \frac{240 \times 280}{22.4 \times 2 \times 1 \times 180} \text{ kg} = 8.33 \text{ kg.}$$

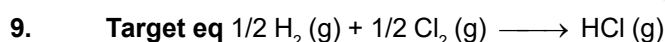
$$7. \quad \text{Heat generated} = C_p \Delta T = 1260 \times 0.667 \text{ cal.}$$

$$\therefore n_{\text{CH}_4} = \frac{1260 \times 0.667}{210 \times 10^3}$$

$$n_{\text{total}} = \frac{PV}{RT} = 4 \times 10^{-2} \quad \therefore \text{mol\%} = \frac{4 \times 10^{-3}}{4 \times 10^{-2}} \times 100\% = 10\% \text{ Ans.}$$

$$8. \quad \Delta H_2 - 24 = -0.024 \times (523 - 473) \text{ Cal/g.}$$

$$\therefore \Delta H_2 = 22.8 \text{ Cal/g.}$$

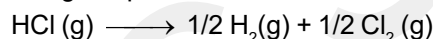


$$\Delta H = \text{eq (6)} - \text{eq (3)} + \text{eq (2)} + \text{eq (4)} + \text{eq (5)}$$

$$= -12.1 - 3.8 - (-75.3) - 11 - 8.8 - 17.5$$

$$= +22.1$$

from this we get equation



$$\therefore \Delta H \text{ of target eq} = -\Delta H = -22.1 \text{ Kcal Ans.}$$

DPP No. # 51

$$1. \quad -372.0 \text{ kCal.} \quad 2. \quad -136.8 \text{ kJ.} \quad 3. \quad -121 \text{ kJ/mole.}$$

$$4. \quad \Delta H = -67710 \text{ Cal} \quad 5. \quad -22 \text{ kCal/mol.}$$

$$6. \quad \text{C}_2\text{H}_4(\text{g}) + \text{H}_2 \longrightarrow \text{C}_2\text{H}_6$$

$$\Delta H = (\Delta H)_{\text{sup}} - (\Delta H)_{\text{req}}$$

$$\Delta H = [145 + 104] - [80 + 2 \times 99]$$

$$\Delta H = -29 \text{ kCal/mol}$$

$$7. \quad \text{C}_2\text{H}_4(\text{s}) \longrightarrow 2\text{C}(\text{o}) + 4\text{H}(\text{g})$$

$$\Delta H_{\text{reaction}} = 4 \times 52.1 + 2 \times 170.9 - 12.5 = 53.7 = \Delta H_{\text{C}=\text{C}} + 4 \times 99$$

$$\Delta H_{\text{C}=\text{C}} = 141.7$$

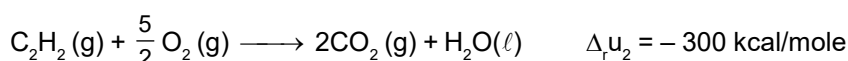
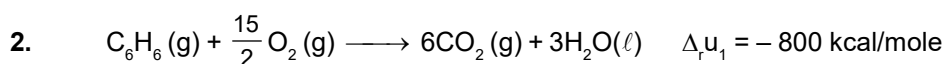
$$8. \quad = \frac{3y - 4x}{3} \text{ kCal mol}^{-1}. \quad 9. \quad 49 \text{ kCal/mol.}$$

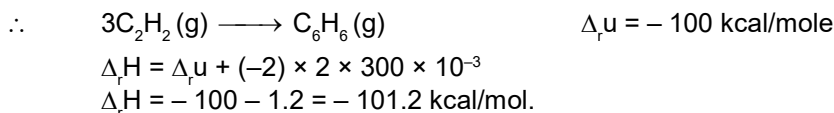
$$11. \quad -49.86 = \Delta H_{\text{ion}} - 55.84$$

$$\Delta H_{\text{ion}} = 55.84 - 49.86 = 5.98 \text{ KJ/mol.}$$

DPP No. # 52

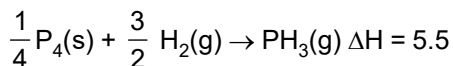
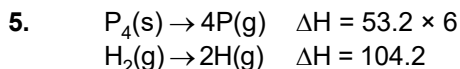
$$1. \quad -41.104 \text{ kCal.}$$





3. 80 kCal/mol.

4. 100 kJ/mol.



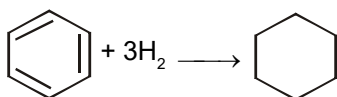
$$\frac{1}{4} \times 6 \times 53.2 + \frac{3}{2} \times 104.2 - 3\epsilon_{\text{P-H}} = 5.5$$

$$\Rightarrow \epsilon_{\text{P-H}} = 76.866 \text{ i.e. } 76.9 \text{ kcal mol}^{-1}$$

6. C - H = 99 kCal ; C - C = 82 kCal

7. -56.5 kJ.

8. -152 KJ mol⁻¹



$$\Delta H_{\text{calculated}} = 3 \times (-119) = -357 \text{ KJ mol}^{-1}$$

$$\Delta H_{\text{experimental}} = \sum (\Delta H_f^\circ)_{\text{product}} - \sum (\Delta H_f^\circ)_{\text{reactant}}$$

$$\text{or } \Delta H_{\text{expt}} = -156 - (49 + 0) = -205 \text{ KJ mol}^{-1}$$

$$\text{Resonance energy} = -357 - (-205) = -152 \text{ KJ mol}^{-1}$$

9. -18.7 kCal

10. -167.2 kJ/mol.

DPP No. # 53

2. Latent heat of fusion of ice per mole = $80 \times 18 = 1440 \text{ cal.}$

Latent heat of vapourisation of liquid water per mole = $596 \times 18 = 10728 \text{ cal.}$

$$\therefore \text{Total } q = (1440 + 10728) \text{ cal} = 12168 \text{ cal.}$$

$$\therefore q_p = \Delta H = 12168 \text{ cal} \quad \text{Ans.}$$

$$\Delta E = \Delta H - P\Delta V = q_p - P\Delta V$$

$V_2 = \text{volume of 1 mole of H}_2\text{O (g) and } V_1 \approx 0.$

$$\therefore P\Delta V = 546 \text{ Cal}$$

$$\therefore \Delta E = (12168 - 546) \text{ cal} = 11622 \text{ Cal.}$$

3. $W = 0.1 \text{ KJ, } q = 2\text{KJ, } DE = 2.1 \text{ KJ.}$

$$4. n_{\text{O}_2}(\text{inhaled}) = \frac{640}{32} = 20$$

12 mole O_2 consumes 1 mole = 342 g sucrose.

$$\therefore \text{Mass of sucrose consumed} = \frac{342}{12} \times 20 \text{ g} = 570 \text{ g.}$$

$$\text{and heat liberated} = \frac{5472}{342} \times 570 \text{ kJ.} = 9120 \text{ kJ.}$$

$$5. \Delta H_{\text{vap}}(0^\circ\text{C}) = \int_{273}^{373} C_p(\text{liquid}) dT + \Delta H_{\text{vap}}(100^\circ\text{C}) + \int_{373}^{273} C_p(\text{gas}) dT$$

$$= 75 \times 100 + 40,000 - 30 \times 100$$

$$= 44,500 \text{ J mole}^{-1} = 44.5 \text{ kJ mole}^{-1}$$

6.
$$\Delta H_{\text{sub}}(223\text{K}) = \int_{223}^{273} C_p(\text{solid}) dT + \Delta H_{\text{fus}}(0^\circ\text{C}) + \int_{273}^{373} C_p(\text{liquid}) dT + \Delta H_{\text{vap}}(100^\circ\text{C}) + \int_{373}^{223} C_p(\text{gas}) dT$$

$$= 50 \times 40 + 6000 + 100 \times 75 + 40000 - 150 \times 30$$

$$= 51 \text{ kJ/mole.}$$
7.
$$\Delta H_2^\circ = \Delta H_1^\circ + \Delta C_p (T_2 - T_1) = 43.285 + (-45 \times 100)$$

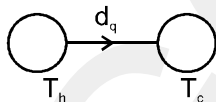
$$= 38785 \text{ J mole}^{-1}.$$
8.
$$\Delta C_p = -ve$$

$$C_{p(\text{products})} < C_{p(\text{Reactants})} \text{ so } q_2 < q_1$$
9.
$$\Delta H_0^2 = [-30 \text{ kJ/mole}] + \{[2 \times 2 \times 17 - 28 - 3 \times 2 \times 10] (100) \text{ J/mole}\}$$

$$= (-30 \text{ kJ/mole}) + (-2000 \text{ J/mole}) = -32 \text{ kJ/mole.}$$

DPP No. # 54

1. Polymerisation leads to more ordered structure.
2. Δn_g is + ve
3. Δn_g is most - ve
4. For same amount of gas at constant temperature, lesser is the volume, lower will be the entropy.
6. For a reversible adiabatic process,
 $\Delta S_{\text{sys}} = \Delta S_{\text{surr}} = \Delta S_{\text{univ}} = 0$
7. For initial state $P_i \times 22.4 = 2 \times R \times 546 \quad \therefore P_i = 4 \text{ atm}$
 Now, $P_i V_i = P_f V_f$ (\therefore process is Isothermal)
 $4 \times 22.4 = 2 \times V_f \quad \therefore V_f = 44.8 \text{ L}$
- $\therefore \Delta S_{\text{sys}} = nR \ln \left(\frac{V_f}{V_i} \right) = 2R \ln \left(\frac{44.8}{22.4} \right) = 2R \ln 2 = R \ln 4$
8. (a)
$$\Delta S_{\text{vap.}} = \frac{\Delta H_{\text{vap.}}}{T} = \frac{26 \times 10^3}{325} = 80 \text{ JK}^{-1} \text{ mol}^{-1}.$$
- (b)
$$\Delta S_{\text{cond.}} = \frac{\Delta H_{\text{cond.}}}{T} = -80 \text{ JK}^{-1} \text{ mol}^{-1}.$$
- 9.



For a small exchange in heat at time 't'

$$\text{change entropy for hot piece} = \frac{dq}{T_h^1}$$

where T_h^1 is temp of hot piece at time 't'

$$\text{change of entropy by cold piece} = \frac{dq}{T_c^1}.$$

As heat capacities of the pieces is same.

$$T_c + T_h = T_c^1 + T_h^1 = 2T_f$$

where T_f is final temperature of each piece.

$$\Delta S \text{ for hot piece} = \int \frac{dq}{T_h^1} = mS \int_{T_h^1}^{T_f} \frac{dT}{T} = mS \ln \frac{T_f}{T_h}$$

$$\Delta S \text{ for cold piece} = mS \ln \frac{T_f}{T_c}.$$

$$\therefore \text{Total } \Delta S = mS \ln \frac{T_f^2}{T_h T_c} = ms \ln \frac{(T_c + T_h)^2}{4T_h T_c}$$

10. For isentropic process $\Delta S_{\text{system}} = 0$

$$\therefore nC_{p,m} \ln \frac{T_2}{T_1} + nR \ln \frac{P_1}{P_2} = 0$$

$$\Rightarrow \ln(P_2) = \frac{5}{2} \times \ln \left(\frac{600}{300} \right) = 1.75 \text{ atm}$$

DPP No. # 55

1. $W = -P_{\text{ext}}(V_f - V_i) = -(1 \text{ atm})(8 - 2) \text{ L} = -6 \text{ L atm}$
 as $q = 0$ so

$$\Delta E = W = n \left(\frac{6}{2} R \right) \left(\frac{P_f V_f}{nR} - \frac{P_i V_i}{nR} \right) \quad \text{Here } \Delta E = nC_V \Delta T$$

$$3(8P_f - 12) = -6$$

$$\text{therefore, } 8P_f = 12 - \frac{6}{3} = 10 \Rightarrow P_f = \frac{5}{4} \text{ atm}$$

$$\text{so, } \frac{T_f}{T_i} = \frac{\frac{5}{4} \times 8}{6 \times 2} = \frac{10}{12}$$

$$\text{so } \Delta S = 3 \frac{12}{300} \ln \left(\frac{10}{12} \right) + \frac{12}{300} \ln 4 = 3.312 \text{ J/K}$$

2. $P^2V = \text{constant} \therefore \left(\frac{nRT}{V} \right)^2 V = \text{constant} \therefore \frac{T^2}{V} = \text{constant}$

$$\therefore \frac{T_1^2}{V_1} = \frac{T_2^2}{V_2} \therefore \frac{(300)^2}{1} = \frac{T_2^2}{4} \therefore T_2 = 600 \text{ K}$$

$$\Delta S_{\text{sys}} = nC_V \ln \frac{T_2}{T_1} + nR \ln \frac{V_2}{V_1} = 2 \times \frac{3R}{2} \ln \left(\frac{600}{300} \right) + 2 \times R \ln \left(\frac{4}{1} \right) = 7R \ln 2$$

$$\therefore X = 7$$

4.* For isothermal free expansion of an ideal gas,

$$\Delta T = 0 \text{ Therefore, } \Delta H = \Delta E = 0$$

Also, $W = 0$ (since $P_{\text{ext}} = 0$)

Therefore, from first law, $q = 0$. Therefore, $\Delta S_{\text{surr}} = 0$.

Since gas is expanding, $\Delta S_{\text{sys}} > 0$.

5. I. Molar entropy of gas is much greater than that of solid and liquid.

II. Entropy change is positive if Δn_g is positive.

III. Molar entropy of a crystalline solid will be zero at absolute zero.

IV. In irreversible process both system and surroundings are not restored if path is reversed.

V. Refractive index and molarity are intensive properties.

7. If $\Delta H < 0$ and $\Delta S < 0$, then reaction is non-spontaneous at high temperatures and spontaneous at low temperatures.

8. $\text{H}_2\text{O}(l, 1\text{bar}, 373\text{K}) \longrightarrow \text{H}_2\text{O}(g, 1\text{bar}, 373\text{K})$

$$\Delta S > 0$$

$$\Delta H > 0$$

$$\Delta G = 0$$

9. $(C_p)_m = aT^3 \therefore 0.375 = a(10)^3 \therefore a = \frac{3}{8} \times 10^{-3}$

$$S_m = \int_0^{20} \frac{(C_P)_m dT}{T} = \int_0^{20} aT^2 dT = \frac{aT^3}{3} \Big|_0^{20} = \frac{8000a}{3} = \frac{8000}{3} \times \frac{3}{8} \times 10^{-3} = 1 \text{ J/K-mol}$$

$$10. \quad \Delta G = nRT \ln \left(\frac{P_f}{P_i} \right) = \left(\frac{144}{18} \right) \times \frac{2}{1000} \times 373 \ln \left(\frac{4}{1} \right) \approx 8 \text{ Kcal.}$$

DPP No. # 56

1. Gram mol. wt. of $C_6H_{12}O_6 = 180 \text{ g}$
i.e. wt. of 6.023×10^{23} molecules = 180

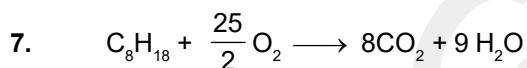
$$\text{so wt. of 1 molecules} = \frac{180}{6.023 \times 10^{23}} = 2.988 \times 10^{-22} \text{ g.}$$

$$2. \quad \text{No. of carbon atom in glucose} = \frac{1.71}{342} \times 12 N_a \\ = 3.6 \times 10^{22}$$

$$4. \quad x \times \frac{0.5}{100} = 78.4 \quad \Rightarrow \quad x = \frac{78.4 \times 10^2}{5 \times 10^{-1}} = \frac{78.4}{5} \times 10^3 = 1.568 \times 10^4.$$

6. At NTP, weight of 1 litre gas = 0.178 gm
so weight of 22.4 litre gas = weight of 1 mole gas = molar mass of gas = $0.178 \times 22.4 \text{ gm}$
vapour density = molar mass of gas / 2

$$\text{so V.D.} = \frac{0.178 \times 22.4}{2} = 2$$



$$M = 1.425 \times 1000 \times 0.8 = 1140 \text{ g}$$

$$\text{mol} = \frac{1140}{114} = 10 \text{ mol}$$

Now from mole-mole analysis

$$\frac{\text{mole of } C_8H_{18}}{1} = \frac{\text{mole of } O_2}{25/2}$$

$$\frac{10}{1} = \frac{\text{mole of } O_2}{25/2} \quad \Rightarrow \quad \text{mole of } O_2 = \frac{25}{2} \times 10 = 125 \text{ mol.}$$



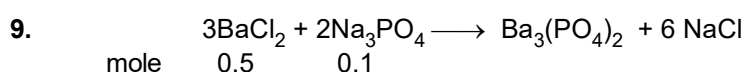
$$\frac{100}{64} \quad (\text{excess})$$

From mole-mole analysis

$$\frac{100}{64} = \frac{n_{C_2H_2}}{1} \quad (\text{here } n = \text{mole})$$

$$\text{vol.} = n_{C_2H_2} \times 22.4 \text{ (at N.T.P.) (N.T.P i j)}$$

$$= \frac{100}{64} \times 22.4 = 35 \text{ lit.}$$



$$\text{mole} \quad 0.5 \quad 0.1$$

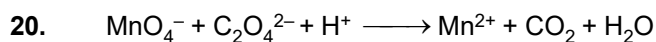
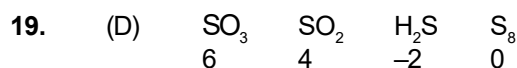
$$\frac{0.5}{3} \quad \frac{0.1}{2} \quad (\text{L.R is } Na_3PO_4)$$

Now from mole-mole analysis vc eksy&eksy fo'ys" k.k ls

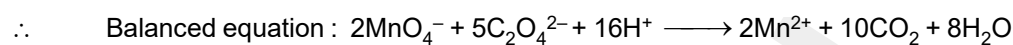
$$\frac{\text{mole of } Na_3PO_4}{2} = \frac{\text{mole of } Ba_3(PO_4)_2}{1}$$

$$\text{NO} \Rightarrow 1(x) + 1(-2) = 0 \therefore x = +2$$

$$\text{N}_2\text{O}_5 \Rightarrow 2(x) + 5(-2) = 0 \therefore x = +5$$



$$\text{V.f.} = 5 \quad \text{V.f.} = 2$$



Topic : Atomic Structure

3. For photoelectric effect to take place, $E_{\text{light}} \geq W \therefore \frac{hc}{\lambda} \geq \frac{hc}{\lambda_0}$ or $\lambda \leq \lambda_0$.

4. More energy means less wavelength.

5. $\text{Power} = \frac{nhc}{\lambda \times t} \Rightarrow 40 \times \frac{80}{100} = \frac{n \times 6.62 \times 10^{-34} \times 3 \times 10^8}{620 \times 10^{-9} \times 20} \Rightarrow n = 2 \times 10^{21}$

9. $r \propto n^2$

11. This is the range of visible region.

12. infrared lines = total lines – visible lines – UV lines = $\frac{6(6-1)}{2} - 4 - 5 = 15 - 9 = 6$.

(visible lines = 4 6→2, 5→2, 4→2, 3→2) (UV lines = 5 6→1, 5→1, 4→1, 3→1, 2→1)

13. For third line of Bracket series (4 → 7)

$$\frac{1}{\lambda} = R \left(\frac{1}{16} - \frac{1}{49} \right) \Rightarrow \lambda = \frac{784}{33R}$$

14. $\lambda = \frac{h}{mv} = 0.4 \times 10^{-33} \text{ cm}$

15. $\lambda = \frac{h}{\sqrt{2mK}} = 3.328 \times 10^{-10} \text{ m}$.

18. Number of radial nodes = $n - \ell - 1 = 1$, $n = 3$. $\therefore \ell = 1$.

$$\text{Orbital angular momentum} = \sqrt{\ell(\ell+1)} \frac{h}{2\pi} = \sqrt{2} \frac{h}{2\pi}$$

19. After np orbital, (n + 1) s orbital is filled.

20. $\text{Rb}_{37} : [\text{Kr}] 5s^2$. $\therefore n = 5, \ell = 0, m = 0, s = \pm \frac{1}{2}$.

DPP No. # 57

1. $PV = \left(P + \frac{1}{100}P \right) V_2$

$$V_2 = \frac{PV}{\frac{101}{100}P} \Rightarrow V_2 = \frac{100}{101}V$$

$$\% \text{ decrease } \frac{1}{4}\% \text{ de} h^{\frac{1}{2}} = \frac{\frac{100}{101}V}{V} = \frac{100}{101}\%$$

2. $V_1 = 100 \text{ ml} \quad V_2 = 80 \text{ ml}$

$$T_1 = 300 \text{ K} \quad T_2 = ?$$

$$P_1 = 740 \text{ mm} \quad P_2 = 740 \text{ mm}$$

Applying Charles law $V \propto T$

$$\frac{V_1}{T_1} = \frac{V_2}{T_2}$$

$$\frac{100}{300} = \frac{80}{T_2}$$

$$T_2 = \frac{300 \times 80}{100} = 240 \text{ K} = 24 - 273 = 240 - 273^\circ\text{C} = -33^\circ\text{C}.$$

3. $V \propto T$ (at constant n and P).

4. Apply Dalton's law of partial pressure

$$\text{Initially} \quad n_1 = \frac{P_1 V}{RT} = \frac{100 \times V}{RT} \quad ; \quad n_2 = \frac{P_2 V}{RT} = \frac{400 \times V}{RT}$$

$$5. \quad P.P_{H_2} = \frac{\frac{w}{2}}{\frac{w}{2} + \frac{w}{16}} \times P \quad \Rightarrow \quad P.P_{H_2} = \frac{8}{9} P$$

$$6. \quad \frac{1}{6} = \sqrt{\frac{2}{x}} \quad (\text{Where } x \text{ is molecular weight of gas})$$

$$\frac{1}{36} = \frac{2}{x}$$

$$x = 72$$

$$7. \quad \frac{r_{H_2}}{r_{O_2}} = \sqrt{\frac{d_{O_2}}{d_{H_2}}}$$

$$\frac{1}{r_{O_2}} = \sqrt{\frac{1.44}{0.09}}$$

$$r_{O_2} = \sqrt{\frac{1}{16}}$$

$$r_{O_2} = \frac{1}{4}$$

$$8. \quad \frac{\frac{50}{20}}{\frac{40}{t}} = \sqrt{\frac{32}{2}}$$

$$\frac{50t}{20 \times 40} = 4$$

$$t = 64 \text{ min.}$$

9. K.E. $\propto T$
(T will same)

$$10. \quad V_{\text{mps}} : V_{\text{av}} : V_{\text{rms}}$$

$$\Rightarrow \sqrt{\frac{2RT}{M}} : \sqrt{\frac{8RT}{\pi M}} : \sqrt{\frac{3RT}{M}} \quad \Rightarrow \quad \sqrt{2} : \sqrt{8/\pi} : \sqrt{3}$$

$$11. \quad \text{Average K.E. for one mole} = \frac{3}{2} RT$$

Average K.E. for 14 g of N_2 $\left(\frac{1}{2}\text{mole}\right) = \frac{3}{2} \times \frac{8.314}{2} \times 400 = 2494 \text{ J.}$

12.
$$\frac{V_{\text{rms,SO}_2}}{V_{\text{rms,He}}} = \sqrt{\frac{T_{\text{SO}_2} \times M_{\text{He}}}{T_{\text{He}} \times M_{\text{SO}_2}}}$$

$$\frac{1}{2} = \sqrt{\frac{T_{\text{SO}_2} \times 4}{300 \times 64}}$$

$$4 = \frac{T_{\text{SO}_2}}{300}$$

$$T_{\text{SO}_2} = 1200 \text{ K}$$

13._ A real gas approaches the behaviour of ideal gas when the pressure is low and the temperature is high.

15._ For ideal gas, compressibility factor (Z) = 1.

16._ $T_c = \frac{8a}{27Rb}$. Thus $T_c \propto \frac{a}{b}$

17. $PV = nRT = \frac{w}{M}RT$

or $P = \frac{w}{V} \frac{RT}{M} = \frac{dRT}{M}$

Thus $P \propto d$, $P \propto T$. Hence,

$$\frac{P_1}{P_2} = \frac{d_1}{d_2} \times \frac{T_1}{T_2} = \frac{1}{2} \times \frac{2}{1} = 1 : 1.$$

18. $U_{\text{rms}} = \sqrt{\frac{3RT}{M}}$ using ideal gas equation,

$$PV = nRT = \frac{w}{M}RT; \quad \frac{RT}{M} = \frac{RV}{w} = \frac{P}{d} \text{ where } d \text{ is the density of the gas}$$

$$\therefore U_{\text{rms}} = \sqrt{\frac{3P}{d}} \text{ at constant pressure, } U_{\text{rms}} \propto \frac{1}{\sqrt{d}}$$

19. Pressure of helium = 8 bar

Pressure of CH_4 = 2 bar

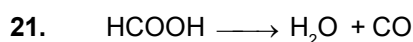
$$\frac{r_{\text{He}}}{r_{\text{CH}_4}} = \frac{P_1}{P_2} \sqrt{\frac{M_{\text{CH}_4}}{M_{\text{He}}}} = \frac{8}{2} \sqrt{\frac{16}{4}} = \frac{8}{1} = 8 : 1$$

20. At constant temperature,

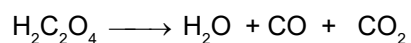
$$P_1 V_1 + P_2 V_2 = P_3 (V_1 + V_2)$$

$$(4.0 \text{ bar})(4.0 \text{ dm}^3) + (6.0 \text{ bar})(6.0 \text{ dm}^3) = P_3 (4.0 + 6.0 \text{ dm}^3)$$

$$\text{or } P_3 = \frac{16 + 36}{10} = \frac{52}{10} = 5.2 \text{ bar.}$$



$$\begin{array}{ccc} \text{a mole} & 0 & 0 \\ & a & a \end{array}$$



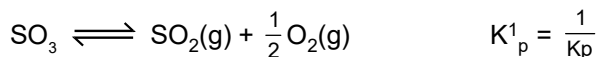
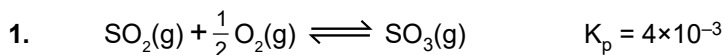
$$\begin{array}{ccc} \text{b mole} & 0 & 0 & 0 \\ & b & b & b \end{array}$$

H_2O absorb by H_2SO_4 and CO_2 absorbed by KOH

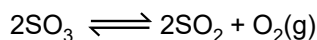
volume of CO_2 / total volume = $b/a + 2b = 1/6$

$$a/b = 4/1$$

the molar ratio of $HCOOH$ and $H_2C_2O_4$ is 4 : 1.

DPP No. # 58


$$K_p^1 = \left(\frac{1}{4 \times 10^{-3}} \right)$$



$$K_p^{\text{II}} = (K_p^1)^2 = \left[\frac{1}{4 \times 10^{-3}} \right]^2 = \left[\frac{1000}{4} \right]^2 = 6250 = 625 \times 10^2 \quad \mathbf{6.25 \times 10^4 \text{ atm.}}$$

2. $\log \frac{K_p}{K_c} + \log RT = 0$

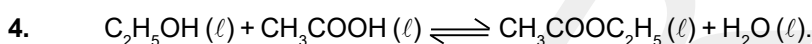
$$\log \left(\frac{K_p}{K_c} \cdot RT \right) = 0$$

$$K_p = K_c (RT)^{-1}$$

$$\therefore K_p = K_c (RT)^{\Delta n} \quad ; \quad \Delta n = -1$$

This is possible one for option (B).

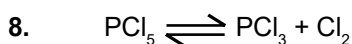
3. Equilibrium const. is temp. dependent only.



a	a	0	0
a - 0.33a	a - 0.33a	0.33a	0.33a

$$K_c = \frac{(0.33a) \times (0.33a)}{(0.67a) \times (0.67a)} = K_c = 1/4.$$

5. Since, K_p is temperature dependent only.



$$\alpha = .2, \text{ initially, } K_p = \frac{\alpha^2}{1 - \alpha^2} P = \frac{(0.2)^2}{1 - (.2)^2} \times 1 = \frac{.04}{.96} = .042$$

$$\text{If } \alpha = .5, \text{ thus, } \frac{(.5)^2}{1 - (.5)^2} \times P = .042, \quad P = .126$$

9. Since inert gas addition has no effect at const. volume.

12. $P_{\text{NH}_3} = P_{\text{H}_2\text{S}} = \frac{P}{2}$ Hence $K_p = P_{\text{NH}_3} \times P_{\text{H}_2\text{S}} = \frac{P}{2} \times \frac{P}{2} = \frac{P^2}{4}$

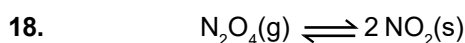
13. At room temperature, $K = 4.32$

and at 425°C , equilibrium constant become 1.24×10^{-4} i.e. it is decreases with increase in temperature. So, it is exothermic reaction.

14. $K = [\text{B}(\text{g})]^2 [\text{C}(\text{g})]^3 = x^2 y^3$. If $[\text{C}(\text{g})]$ is doubled i.e. = $2y$. Suppose $[\text{B}(\text{g})]$ is z . Then

$$K = z^2 (2y)^3 = x^2 y^3 \quad \text{or} \quad z^2 = \frac{1}{8} x^2 \quad \text{or} \quad z = \frac{1}{\sqrt{8}} x = \frac{1}{2\sqrt{2}} x.$$

17. On mixing some quantity of 0.01 M HCl in aqueous solution of CH_3COOH , equilibrium concentration of CH_3COO^- will be increase.



t = 0 0.1 mole 0

t = eq 0.05 0.1

$$k = \frac{(0.1)^2}{0.05} = 0.2$$

19. $\text{PCl}_5(\text{g}) \rightleftharpoons \text{PCl}_3(\text{g}) + \text{Cl}_2(\text{s})$
 at eq, mole of $\text{PCl}_3 = \text{mole of Cl}_2$

$$\text{So } K = \frac{[\text{PCl}_3][\text{Cl}_2]}{[\text{PCl}_5]} = \frac{\left[\frac{0.2}{10}\right]\left[\frac{0.2}{10}\right]}{\frac{0.1}{10}} = 0.04$$

DPP No. # 59

2. First law of thermodynamics is the law of conservation of energy.

4. Work done by the gas in the cyclic process = Area bounded (ABCA) = $5P_1V_1$

6. From I law of thermodynamics $\Delta E = Q + W$
 where $Q = 0$ for adiabatic process.

7. $\Delta U = W$

$$nC_v(T_2 - T_1) = -P \times (V_2 - V_1)$$

$$\frac{3}{2} R(T_2 - T_1) = -1 \quad \Rightarrow \quad \therefore T_2 = T_1 - \frac{2}{3 \times 0.0821}$$

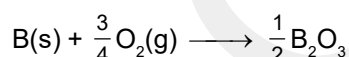
8. $q = 0 \quad \therefore \Delta U = w$

$$\Rightarrow nC_{v,m}(T_2 - T_1) = -P_{\text{ext}} \left[\frac{nRT_2}{P_2} - \frac{nRT_1}{P_1} \right]$$

$$\therefore C_{v,m}(T_2 - T_1) = P_{\text{ext}} \cdot R \left[\frac{T_1}{P_1} - \frac{T_2}{P_2} \right] \Rightarrow \frac{3}{2} R [T_2 - 300] = 2 \times R \left[\frac{300}{5} - \frac{T_2}{2} \right] \Rightarrow T_2 = 228 \text{ K}$$

9. When one mole of NH_3 is formed from its constituent elements the enthalpy change = -46.0 kJ
 Therefore when one mole of NH_3 decompose to give its constituent elements enthalpy change = 46.0 kJ
 \Rightarrow When 2 mole NH_3 decompose, enthalpy change = $2 \times 46 = 92.0 \text{ kJ}$

10. Combustion reaction of solid boron

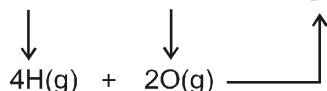


$$\Delta H_r^\circ = \Delta H_c^\circ = \frac{1}{2} \Delta H_f^\circ(\text{B}_2\text{O}_3, \text{s}) - \Delta H_f^\circ(\text{B}, \text{s}) - \frac{3}{4} \Delta H_f^\circ(\text{O}_2, \text{g})$$

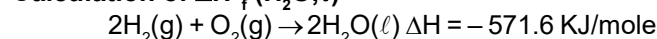
ΔH_f° of element in stable state of aggregation is assumed to be zero.

$$\Delta H_c^\circ = \frac{1}{2} \Delta H_f^\circ(\text{B}_2\text{O}_3)$$

11. (1) $\text{H}_2\text{O}(\ell) \longrightarrow \text{H}_2\text{O}(\text{g}) \quad \Delta H = 40.6 \text{ KJ/mole}$
 (2) $2\text{H}(\text{g}) \longrightarrow \text{H}_2(\text{g}) \quad \Delta H = -435.0 \text{ KJ/mole}$
 (3) $\text{O}_2(\text{g}) \longrightarrow 2 \text{O}(\text{g}) \quad \Delta H = -49836 \text{ KJ/mole}$
 (4) $2\text{H}_2(\text{g}) + \text{O}_2(\text{g}) \longrightarrow 2\text{H}_2\text{O}(\ell) \quad \Delta H = -571.6 \text{ KJ/mole}$



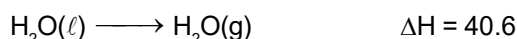
- (1) **Calculation of $\Delta H_f^\circ(\text{H}_2\text{O}, \ell)$**



$$\Delta H_r^\circ = 2\Delta H_f^\circ(\text{H}_2\text{O}, \ell) - 2\Delta H_f^\circ(\text{H}_2, \text{g}) - \Delta H_f^\circ(\text{O}_2, \text{g})$$

$$\begin{array}{ccc} \downarrow & & \downarrow \\ \text{Zero} & & \text{Zero} \\ -571.6 = 2\Delta H_f^\circ(\text{H}_2\text{O}, \ell) & \text{so} & \Delta H_f^\circ(\text{H}_2\text{O}, \ell) = -285.5 \end{array}$$

(2) Calculation of $\Delta H_f^\circ(\text{H}_2\text{O}, \text{g})$

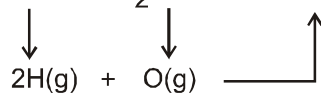


$$\Delta H_f = \Delta H_f^\circ(\text{H}_2\text{O}, \text{g}) - \Delta H^\circ(\text{H}_2\text{O}, \ell)$$

$$\Delta H_f^\circ(\text{H}_2\text{O}, \text{g}) = \Delta H_f^\circ(\text{H}_2\text{O}, \ell) + \Delta H_r$$

$$= -285.8 + 40 = -245.8$$

(3) $\text{H}_2(\text{g}) + \frac{1}{2}\text{O}_2(\text{g}) \longrightarrow \text{H}_2\text{O}(\text{g}) \quad \Delta H = -245.8$



$$\Delta H_r = \epsilon_{\text{H-H}} + \frac{1}{2} \epsilon_{\text{O-O}} - 2 \epsilon_{\text{O-H}} \Rightarrow -245.8 = +435 + \frac{1}{2}(489.6) - 2 \times \epsilon_{\text{O-H}}$$

$$2\epsilon_{\text{O-H}} = 435 + 244.8 + 245.8 \Rightarrow 2\epsilon_{\text{O-H}} = 925.6$$

$$\epsilon_{\text{O-H}} = \mathbf{462.5}$$

13. $n\text{CH}_2 = \text{CH}_2 \longrightarrow (-\text{CH}_2 - \text{CH}_2)_n \quad \Delta H = -100 \text{ KJ/mole}$

$$n[\text{C} = \text{C}] + n[\text{C} - \text{H}]4 - n[\text{C} - \text{H}]4 - n[\text{C} - \text{C}] \times 2 = -100$$

$$n[\text{C} = \text{C}] - 2n[\text{C} - \text{C}] = -100 \Rightarrow [\text{C} = \text{C}] - 2[\text{C} - \text{C}] = -100$$

$$\Rightarrow +600 - 2[\text{C} - \text{C}] = -100 \Rightarrow -2[\text{C} - \text{C}] = -700 \text{ KJ/mole} \Rightarrow (\text{C} - \text{C}) = -350$$

14. Process is Reversible and adiabatic ($Q = 0$)

$$\text{So, } \Delta S = 0$$

15.* Process is endothermic i.e., $\Delta H = +ve$ and process is also spontaneous i.e., $\Delta G = -ve$

Hence, from Gibbs-Helmholtz equation

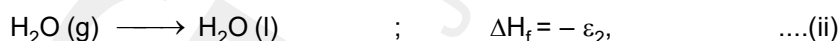
$$\Delta G = \Delta H - T.\Delta S$$

ΔS must be positive so that ΔG may be negative.

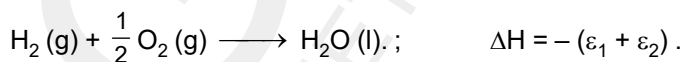
16.* It is because of the fact that for spontaneity, the value of $\Delta G = (\Delta H - T\Delta S)$ should be < 0 . If ΔH is $-ve$, the value of

$T\Delta S$ shall have to be less than ΔH or the value of ΔS has to be less than $\frac{\Delta H}{T}$ i.e., $\frac{x}{298}$.

18. The assertion that the increase in internal energy for vaporisation of one mole of water at 1 atm and 373 K is zero is true because for all isothermal process change in internal energy is zero.



and (i) and (ii).

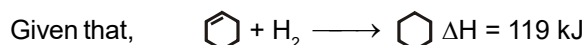


20. Heat of neutralisation for strong acid and strong base combination is constant is equal to -13.7 Kcal or -57.1 KJ .

22. Enthalpy of formation of 3 carbon-carbon double bonds

$$= \Delta H_f(\text{Cyclohexene}) - \Delta H_f(\text{Benzene})$$

$$= -156 - (+49) \text{ kJ} = -205 \text{ kJ}.$$



Theoretical enthalpy of formation of 3 double bonds in benzene ring

$$= 3 \times (-119) \text{ kJ} = -357 \text{ kJ}.$$

$$\therefore \text{resonance energy of benzene} = -357 - (-205) \text{ kJ} = -152 \text{ kJ mole}^{-1} \text{ ®}$$